

SANDIA REPORT

SAND2000-8261
Unlimited Release
Printed December 2000

The Effects of Temperature and Carbon Tetrachloride on Polymer Based Hydrogen Getters

George M. Buffleben, Timothy J. Shepodd

Prepared by
Sandia National Laboratories
Albuquerque, New Mexico 87185 and Livermore, California 94550

Sandia is a multiprogram laboratory operated by Sandia Corporation,
a Lockheed Martin Company, for the United States Department of
Energy under Contract DE-AC04-94AL85000.

Approved for public release; further dissemination unlimited.



Issued by Sandia National Laboratories, operated for the United States
Department of Energy by Sandia Corporation.

NOTICE: This report was prepared as an account of work sponsored by an agency of the United States Government. Neither the United States Government, nor any agency thereof, nor any of their employees, nor any of their contractors, subcontractors, or their employees, make any warranty, express or implied, or assume any legal liability or responsibility for the accuracy, completeness, or usefulness of any information, apparatus, product, or process disclosed, or represent that its use would not infringe privately owned rights. Reference herein to any specific commercial product, process, or service by trade name, trademark, manufacturer, or otherwise, does not necessarily constitute or imply its endorsement, recommendation, or favoring by the United States Government, any agency thereof, or any of their contractors or subcontractors. The views and opinions expressed herein do not necessarily state or reflect those of the United States Government, any agency thereof, or any of their contractors.

Printed in the United States of America. This report has been reproduced directly from the best available copy.

Available to DOE and DOE contractors from
Office of Scientific and Technical Information
P.O. Box 62
Oak Ridge, TN 37831

Prices available from (703) 605-6000
Web site: <http://www.ntis.gov/ordering.htm>

Available to the public from
National Technical Information Service
U.S. Department of Commerce
5285 Port Royal Rd
Springfield, VA 22161

NTIS price codes
Printed copy: A03
Microfiche copy: A01



SAND2000-8261
Unlimited Release
Printed December 2000

The Effects of Temperature and Carbon Tetrachloride on Polymer Based Hydrogen Getters

George M. Buffleben and Timothy J. Shepodd
Materials Chemistry Department
Sandia National Laboratories
Livermore, California 94550

Abstract

This report summarizes hydrogen pumping by organic getters in the presence of carbon tetrachloride, and how the reduction of pumping in the presence of this catalyst poison can be minimized through the choice of catalyst. Catalyst A is shown to be preferred in a clean environment, and catalyst B for a poisoned environment. Additionally, we examine the effects of temperature on pumping rates, and show that this getter is effective over a large temperature range from -23 to 107 degrees Celsius.

The Effects of Temperature and Carbon Tetrachloride on Polymer Based Hydrogen Getters

Introduction

Polymer based getters were invented at Sandia National Laboratories and are produced commercially for consumer and industrial products where hydrogen accumulation is a safety concern. This report discusses the results of hydrogen gas removal (pumping) tests performed at Sandia National Laboratories. These tests were conducted to see how organic getters would perform in the presence of a gas that would poison the getters' catalyst. The tests were conducted with two hydrogen getters that differed only in the catalyst composition (A or B). The getters were forced to compete with each other for a limited amount of hydrogen to determine which catalyst performed better when exposed to different gas mixtures. We also examined the effects of temperature on pumping rates, using getter made with catalyst A.

Experiments

The gas handling apparatus (Figure 1) has been used extensively by Sandia for evaluation of numerous getters. We have a high degree of confidence in the accuracy of the results obtained from this apparatus. However, since the stainless steel apparatus is opened to the air on a daily basis, high vacuum measurements are limited by our ability to degas the reactor of absorbed atmospheric species. As a practical matter, vacuum levels ≤ 0.01 torr require that extra attention be paid to the degas cycle. We are unable to bake out the entire apparatus, so we typically operate with a few millitorr of residual gas during long experiments with sealed volumes. The apparatus includes both a 1000 torr and 10 torr MKS pressure heads manufactured by Baratron. Data is acquired with a LabView NB-MIO-16XL data acquisition card in a Macintosh II ci running LabView V3.1. The digital resolution of the NB-MIO-16XL is 16 bits. With the system logging a data point at least every 10 minutes, we have a maximum pumping rate sensitivity of 1.5×10^{-7} std. cc s⁻¹.

Testing was done on two getters that differed only in the catalyst used (A or B). A 1.00 gram sample of getter powder was loaded into a test tube. A Kimwipe was taped over the opening of the test tube to avoid powder dispersion. The getter samples were degassed at 100 °C for at least 2 hours 10 minutes, as recommended by Vacuum Energy, Inc., before being dosed with the appropriate gas.

To better compare the two getters a second set of experiments was conducted in which the getters were allowed to compete for available hydrogen in the apparatus. Four polypropylene containers (two of each getter) were loaded with 75 to 85 mg of getter each. A Kimwipe was then taped over each container to avoid powder dispersion. The four containers were taped together and loaded into the reactor. Getter masses were matched within a given experiment. The samples were sealed in the reactor and degassed at 100 °C for 2 hours 10 minutes. They were then exposed to hydrogen, or diluted hydrogen, with pressure changes recorded by the computer.

NMR was used to determine how much hydrogen each sample absorbed. NMR samples were prepared by mixing excess quantity of chloroform-d with the getter to dissolve the organic component, and then filtering through magnesium sulfate and a 0.45 µm PTFE filter to dry the sample and remove particles. A Varian Gemini 300 MHz NMR was used to acquire a proton spectrum. The relative integrals of the single and double bond regions were used to calculate the hydrogen uptake of the getters. Hydrogen pumping rates were calculated from the pressure change data, and are average rates for the pressure drop from 90 to 25 torr.

For hydrogen pumping rates at different temperatures, a 1.02 gram powder sample of catalyst A getter was loaded into a test tube and a Kimwipe was taped over the opening. The sample was loaded into a reactor and degassed at 100 °C for 2 hours 10 minutes. Volume A (Figure 2) was filled with \approx 19 torr of hydrogen. Volumes A and E were chilled to -23 °C using an o-xylene/liquid nitrogen bath. The hydrogen was then exposed to the sample, and pressure changes were recorded by the computer. This experiment was repeated four more times using the same getter sample and pumping off any remaining gas between experiments. The second run was done with an ice water bath, and for the last two runs volume E was wrapped in heating tape. Hydrogen pumping rates were calculated from the pressure change data, and are average rates for the pressure drop from 10 to 7 torr.

Argon was purchased from Matheson Tri-gas, while 99.99999% pure hydrogen was produced with a Whatman hydrogen generator model 75-30, and carbon tetrachloride was purchased from Aldrich. Experiments using different concentrations of these gasses were made by mixing the gasses in the apparatus and are reported as mole percent.

Results

We are interested in how the polymer base getters perform when exposed to a gas that poisons the catalyst and how different catalysts effect getter performance. We made two getters that were identical except for the catalyst used (A or B). We chose carbon tetrachloride as the poison because chlorinated hydrocarbons are known to be strong

poisons for these getters. The greater the chlorine content in the poison molecule, the greater the effect on the getter catalyst. Initial tests on each getter were done with a surplus of pure hydrogen. However, the results were difficult to compare since the hydrogen pumping rates were limited only by diffusion through the getter, and were nearly equal. To gain a better understanding of how the choice of catalyst affects the performance of the getters, we set up a competition between them in which both getters were placed into the same reactor and given a dose of hydrogen which was much less than theoretical capacity. The amount of hydrogen absorbed by each getter was quantified by ^1H NMR. In the next two tests, the samples were dosed with 10% and 20% of the getters' theoretical capacity using pure hydrogen. The A getter outperformed the B getter by adsorbing 3.4 and 2.6 times as much hydrogen, respectively.

In the next series of four tests the samples were exposed to a gas mixture containing argon or carbon tetrachloride mixed with hydrogen equal to 20% of the getters capacity. Argon was chosen as an inert control gas and slows the absolute pumping rate as a diluent, but does not change the relative reaction rates (Table 1). The carbon tetrachloride made a significant difference in the performance of the getters. With an atmosphere containing only 0.17% CCl_4 , the A getter removed 1.5 times as much hydrogen as the B getter, and with 14.7% CCl_4 , the A getter pumping dropped to 0.21 times as much hydrogen as the B getter. This clearly shows that while getter made with catalyst A will generally perform better under normal circumstances, in a poisoned environment getter B would be a superior choice.

Gas Composition	Ratio of hydrogen removed (A:B)
H_2 (10% getters' capacity)	3.4
H_2	2.6
0.15% Ar in H_2	2.5
14.7% Ar in H_2	2.4
0.17% CCl_4 in H_2	1.5
14.7% CCl_4 in H_2	0.21

Table 1: Ratio of hydrogen removed by getter A to hydrogen removed by getter B. Amount of hydrogen used is 20% of getters' capacity unless stated otherwise.

One should also look at the hydrogen pumping rates during these tests (Figure 3). In comparing the rates for hydrogen uptake in hydrogen/argon mixtures one can see a drop in the rate (Table 2) as expected due to diffusion of hydrogen through argon. A greater drop in rate can be seen in the samples exposed to carbon tetrachloride due to poisoning of the catalyst as well as diffusion of hydrogen through carbon tetrachloride. Finally, it should be noted that the pressure in experiments with carbon tetrachloride drops below the theoretical pressure predicted for the amount of carbon tetrachloride in the apparatus. This indicates that some of the carbon tetrachloride is absorbed by the getter.

Gas Composition	Hydrogen removal rate (std cc H_2 s^{-1} g^{-1})
H_2	1.1×10^{-2}
0.15% Ar in H_2	9.0×10^{-3}
14.7% Ar in H_2	5.7×10^{-3}
0.15% CCl_4 in H_2	6.2×10^{-3}
14.7% CCl_4 in H_2	2.2×10^{-4}

Table 2: Hydrogen removal rates for getters exposed to gas mixtures. Rates are averages from 90 to 25 torr.

In a second set of experiments we looked at the performance of getter A at different temperatures (Figure 4). A 1.02 gram sample was placed into the reactor and degassed at 100 °C for 2 hours 10 minutes. The reactor was cooled or heated to the desired temperature, and the sample exposed to a small amount of hydrogen. The same sample was used in this series of tests and any remaining gas was pumped off between each test. The capacity of the getter used in each test was so small ($\approx 2\%$) that the rate was essentially unaffected by the reduction in capacity. The lowest temperature had the slowest adsorption rate, and the rate increased with temperature, as expected.

Temperature (°C)	Hydrogen removal rate (std cc H ₂ s ⁻¹ g ⁻¹)
-23	2.4×10^{-4}
1	1.5×10^{-3}
19	6.5×10^{-3}
70	5.0×10^{-2}
107	6.8×10^{-2}

Table 3: Average hydrogen removal rate for getter A from 90 to 25 torr.

Exact values of pumping rates can vary between experiments. Gas uptake rate is sensitive to pressure, temperature, other atmospheric constituents, hydraulic restrictions, physical placement of the getter, and degassing history. Pumping rates should only be compared when generated in the exact same apparatus or when the differences caused by changing apparatuses are quantified. The authors highly recommend testing pumping rates under conditions representative of the actual deployment.

Conclusion

Chlorinated hydrocarbons poison the getter, but do not stop hydrogen pumping completely. The getter still removes hydrogen at a reduced rate even when the poison concentration is as high as 14.7%. The effect of carbon tetrachloride can be minimized through appropriate choice of a catalyst. Catalyst A is best suited for getters not expected to see any poisons; catalyst B should be used for getters in poisoned environments. A mix of the two catalysts may make for a good general getter with a broader range of operating environments.

Pumping rates for getter A were measured at different temperatures. The getter performs well over a large temperature range (-23 to 107 °C), although over this temperature range the pumping rate changes by more than two orders of magnitude. The getters' performance in a particular application will depend on a number of factors including hydrogen generation rate, amount of getter, temperature, poisons, and hydrogen diffusion through other gases.

References

4. Shepodd, T. J.; Phillip, B. L. U.S. Patent 5 624 598, 1997.
5. Shepodd, T. J.; Whinnery, L. L. U.S. Patent 5 837 158, 1998.
3. Shepodd, T. J.; Whinnery, L. L. U.S. Patent 6 063 307, 2000.
4. Shepodd, T. J.; Tichenor, M. S. "Organic Hydrogen Getters for Use in Heat Pipes," Sandia Technical Report SAND99-8218, Sandia National Laboratories, Albuquerque, NM, 87185, April 1999.
5. Schicker, J. R.; "Getter Materials Product Development: DEB Hydrogen Getter Gas Inhibition Analysis," Technical Report: Allied Signal/Kansas City Division Project Number: EPN-047620, May 1995.

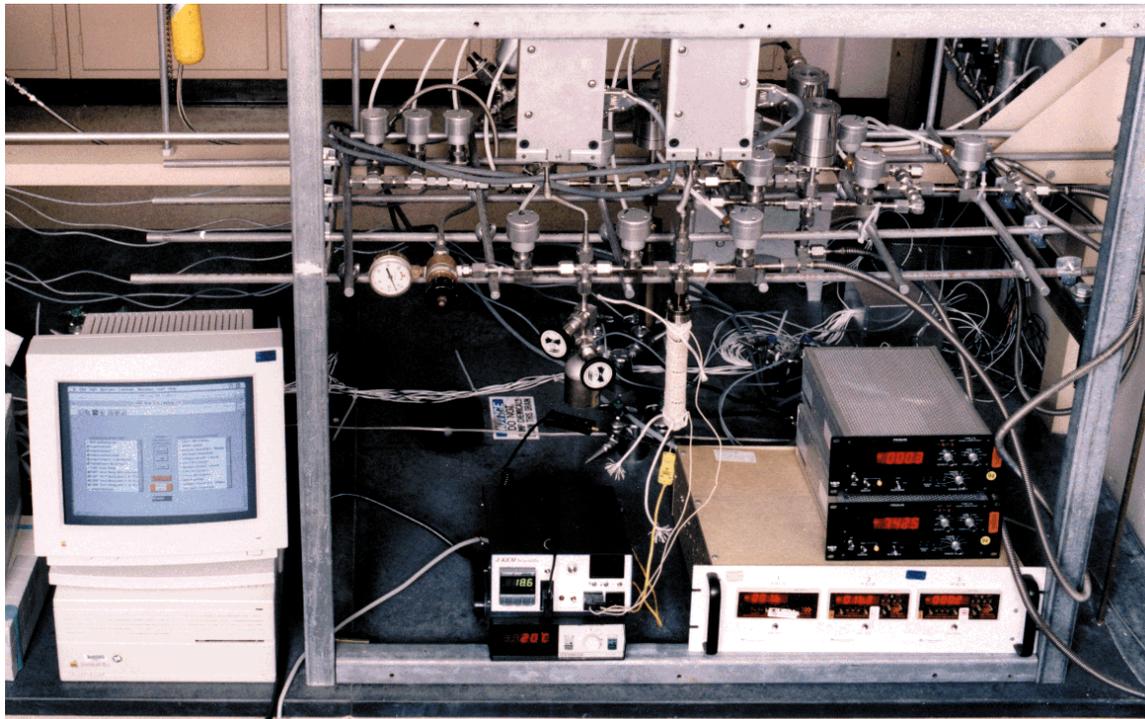


Figure 1. A photograph of the Sandia getter testing apparatus.

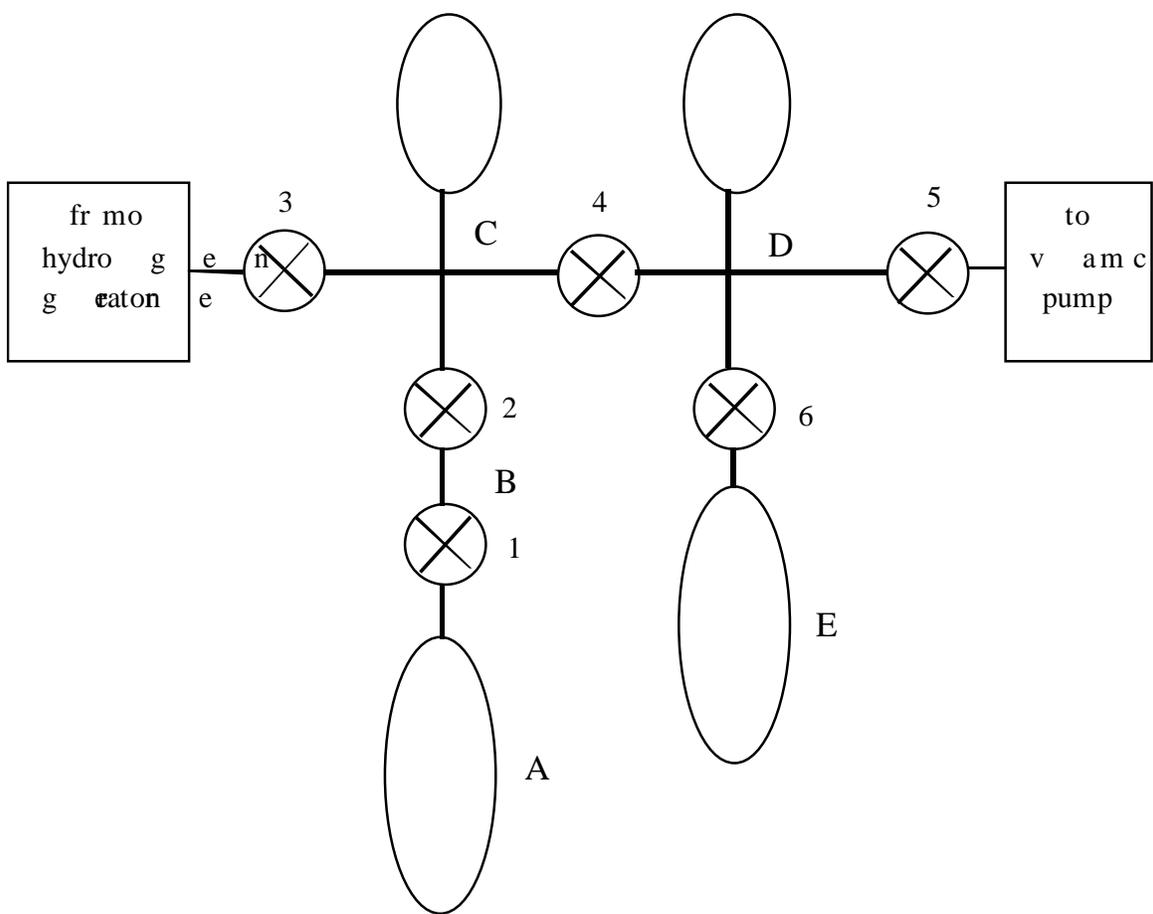


Figure 2. Schematic of apparatus. The volumes of the apparatus are as follows.

A	102.5 ml
B	3.9 ml
C	15.2 ml
D	18.5 ml
E	39.0 ml

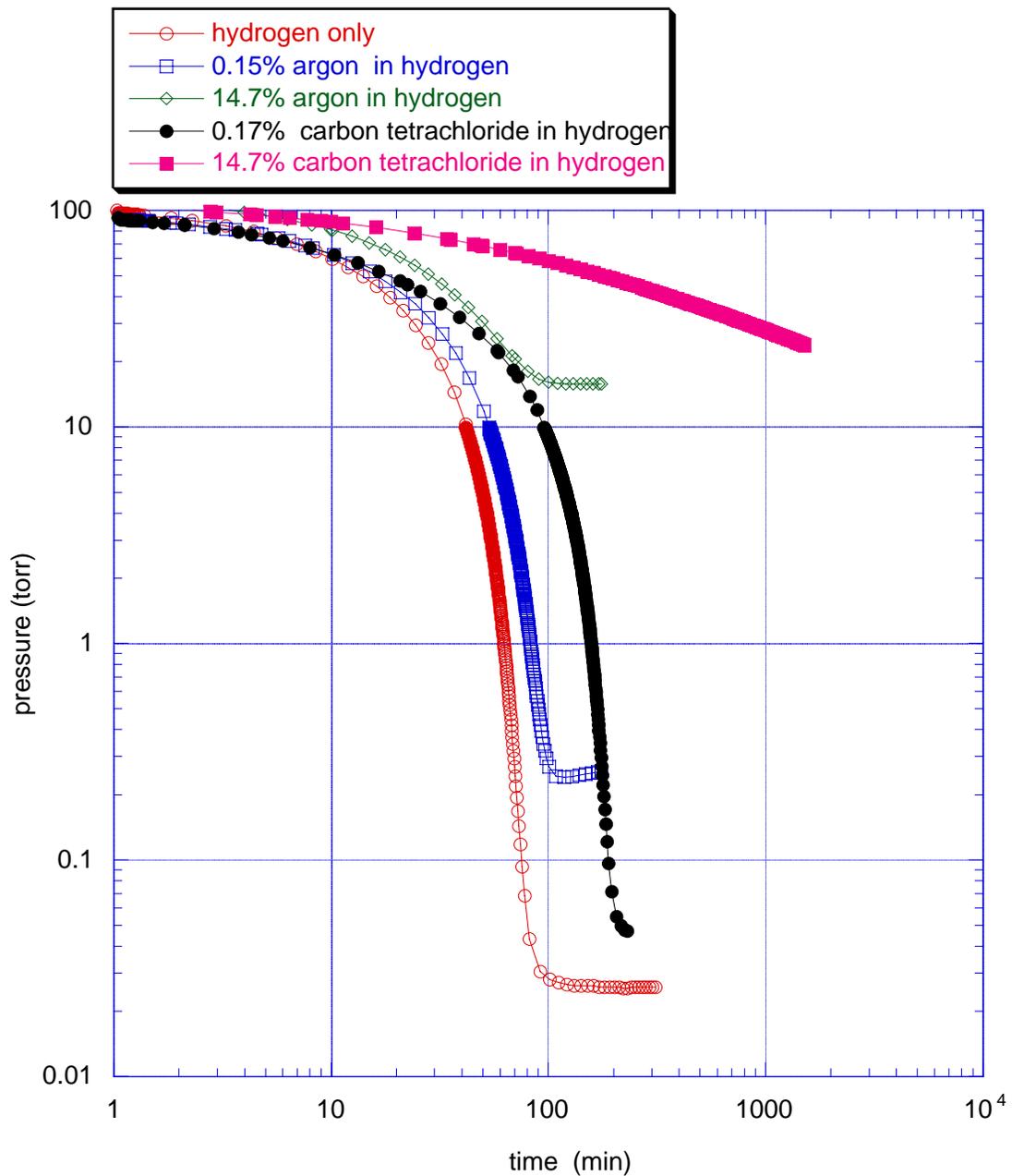


Figure 3. Pressure plot for getter competition experiments.

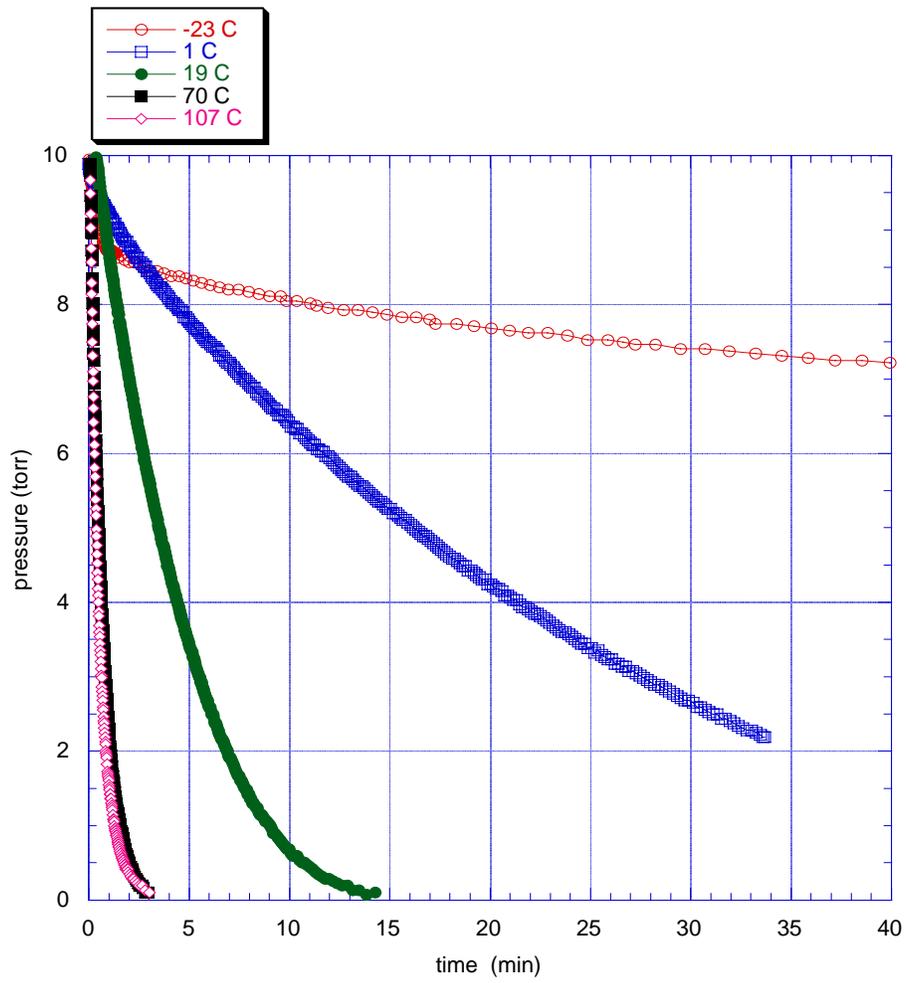


Figure 4. Pressure plot for getter A at different temperatures.

Distribution:

1	MS 9001	M. E. John, 8000 Attn: R. C. Wayne, 2200, MS 9005 J. Vitko, 8100, MS 9004 W. J. McLean, 8300, MS 9007 D. R. Henson, 8400, MS 9007 K. E. Washington, 8900, MS 9003
10	MS 9402	G. M. Buffleben, 8722
1	MS 9402	T. J. Shepodd, 8722
1	MS 9405	T. M. Dyer, 8700 Attn: K. Wilson, 8722, MS 9402
3	MS 9018	Central Technical Files, 8940-2
1	MS 0899	Technical Library, 4916
1	MS 9021	Classification Office, 8311/ Technical Library, MS 0899, 4916
1	MS 9021	Classification Office, 8311/For DOE/OSTI

This page left intentionally blank